

ITP 329

Pump Service & Maintenance  
2017

Troubleshooting with Pump Curves and  
Pressure Gauges

# Problem 1

The system is in operation, but you don't know the flow. From the nameplate you determine the pump is a Series 1510 1-1/4"BC with a 8" diameter impeller operating at 1150 RPM (6 pole motor).

Using a pressure gauge you get the following information:

Suction Pressure	=	12.0 psi
Discharge pressure	=	<u>22.5 psi</u>

Determine the flow.

# Problem 1

Answer:

Differential Gauge Reading:  $22.5\text{psi} - 12\text{psi} = 10.5\text{psi}$

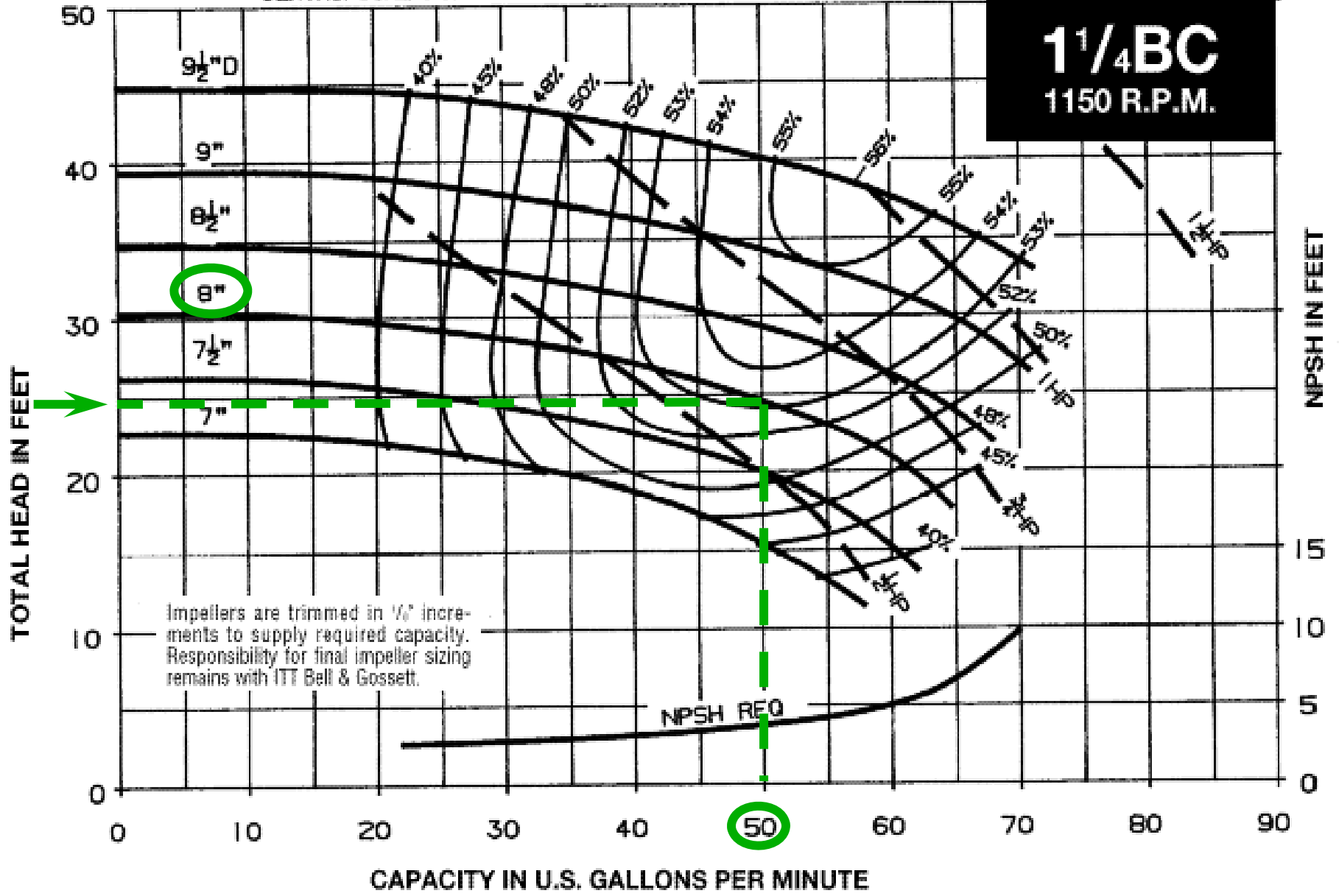
Convert to ft.:  $10.5\text{psi} \times 2.31\text{ft/psi} = 24.3\text{ft}$

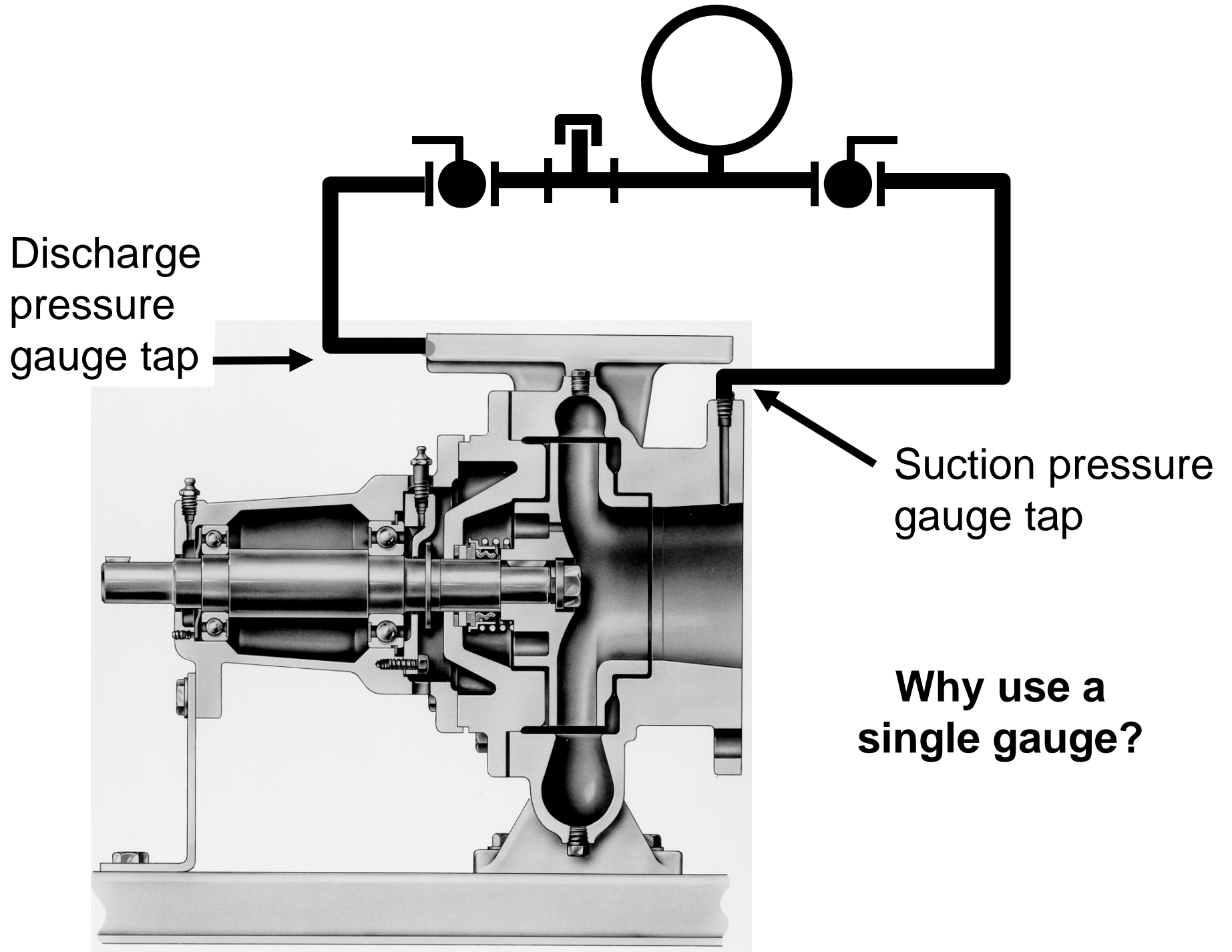
Flow?

CENTRIFUGAL PUMP SERIES 1510

Approved  Date 7-7-61

**1 1/4 BC**  
1150 R.P.M.





Discharge  
pressure  
gauge tap

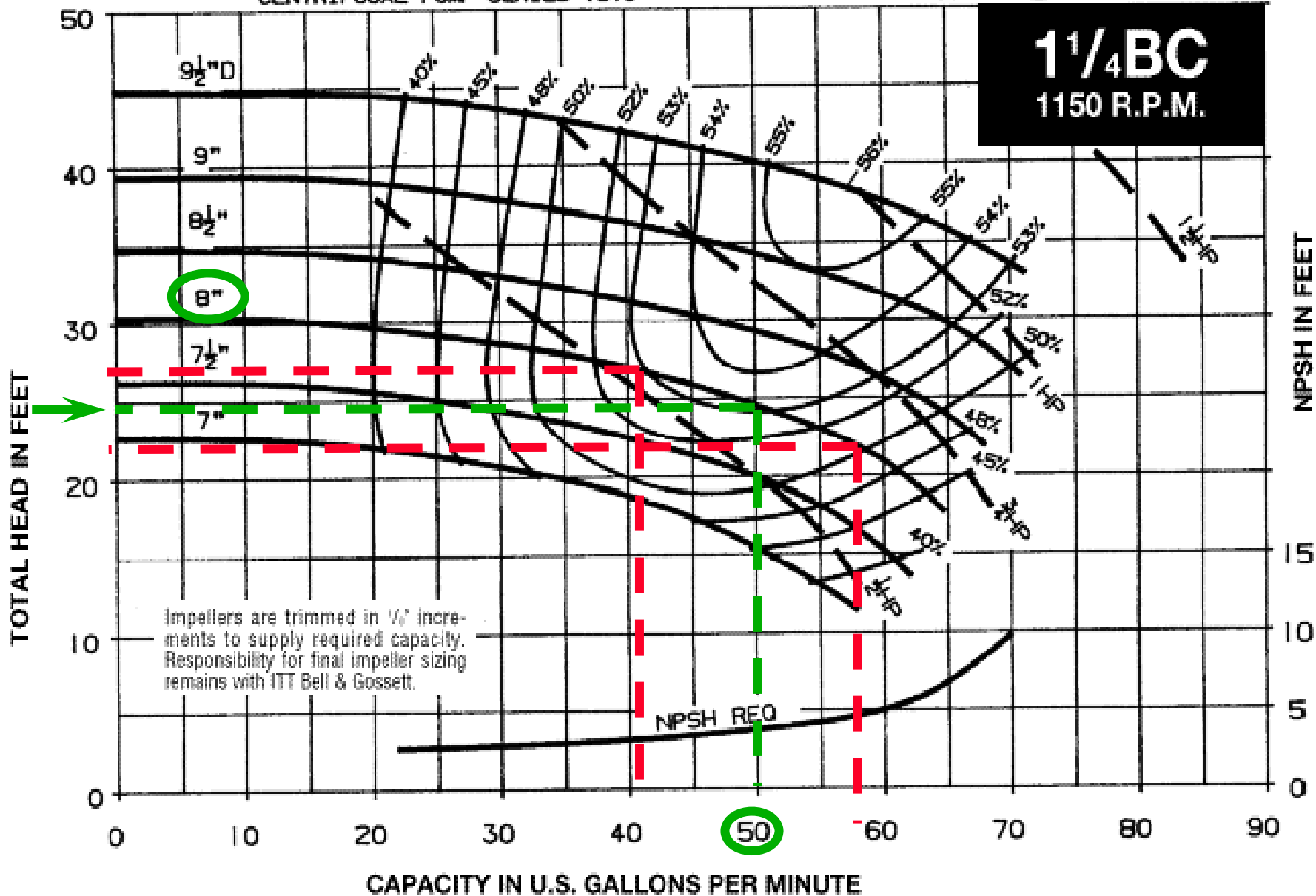
Suction pressure  
gauge tap

**Why use a  
single gauge?**

CENTRIFUGAL PUMP SERIES 1510

Approved  Date 7-7-81

**1 1/4 BC**  
1150 R.P.M.



## Problem 2

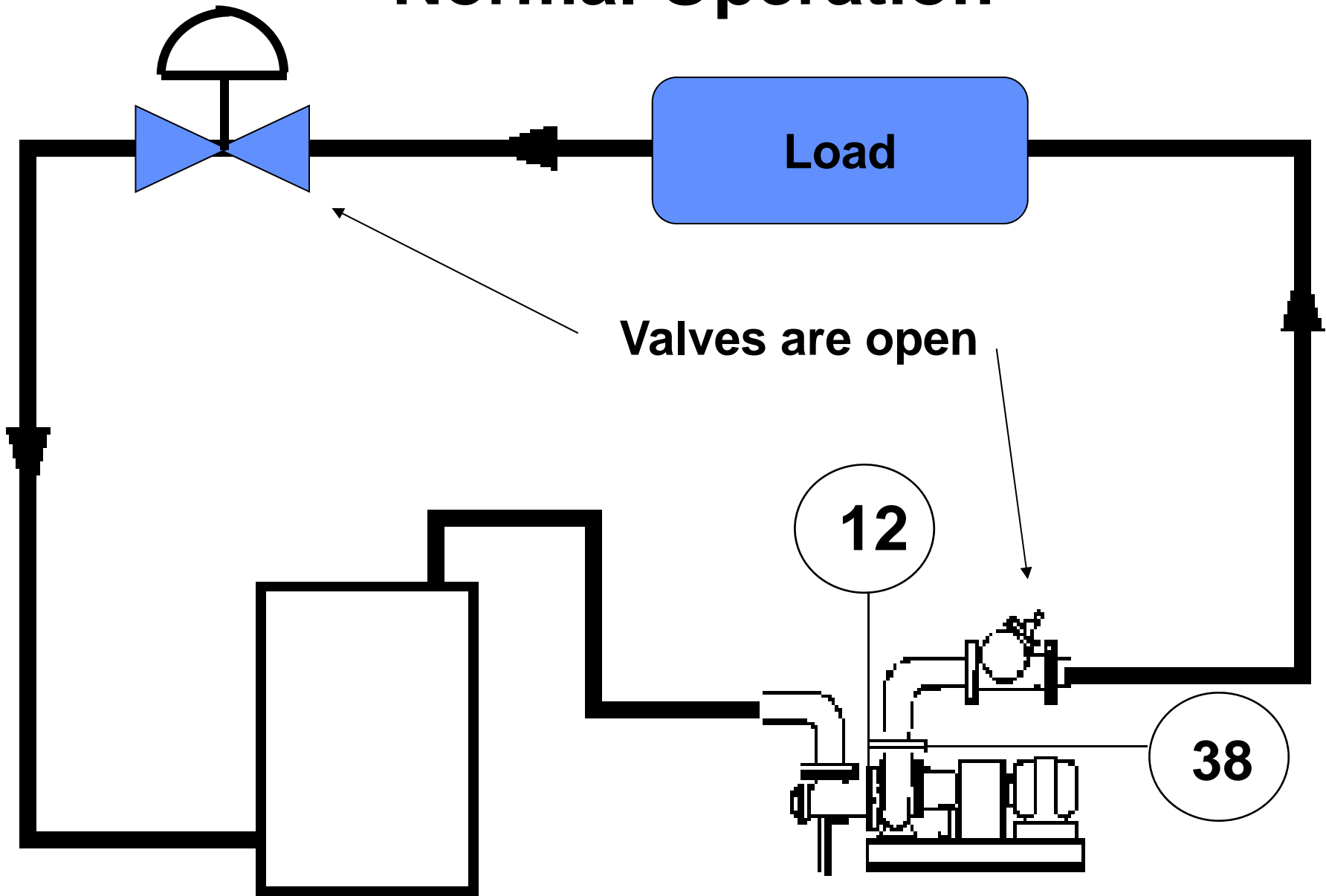
Using a pressure gauge you measure the pressure drop across the pump of your chilled water system. You get the following information:

$$\begin{array}{lcl} \text{Suction pressure} & = & 12\text{psi} \\ \text{Discharge pressure} & = & \underline{38\text{psi}} \end{array}$$

You look at the nameplate on the pump. All you can read is it's a Series 1510 Model 4BC and the motor operates at 1750 RPM.

What's the flow?

# Normal Operation



## Problem 2

Pressure differential across pump during normal operation:

Answer:

Differential Gauge Reading:

$$38\text{psi} - 12\text{psi} = 26\text{psi}$$

Convert to ft.:

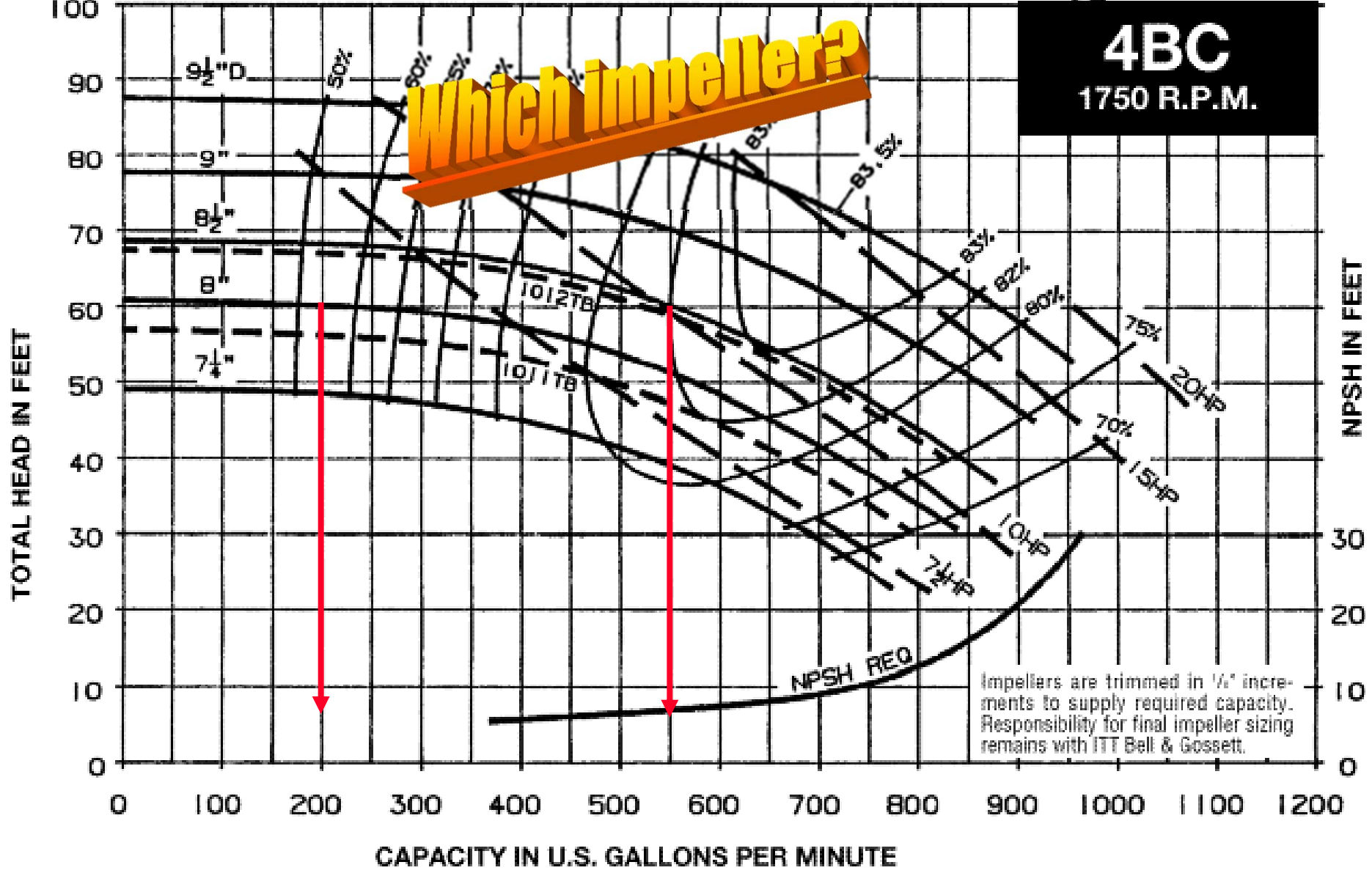
$$26\text{psi} \times 2.31\text{ft/psi} = 60\text{ft}$$

CENTRIFUGAL PUMP SERIES 1510

Approved  Date 3-18-81

**4BC**  
1750 R.P.M.

**Which impeller?**



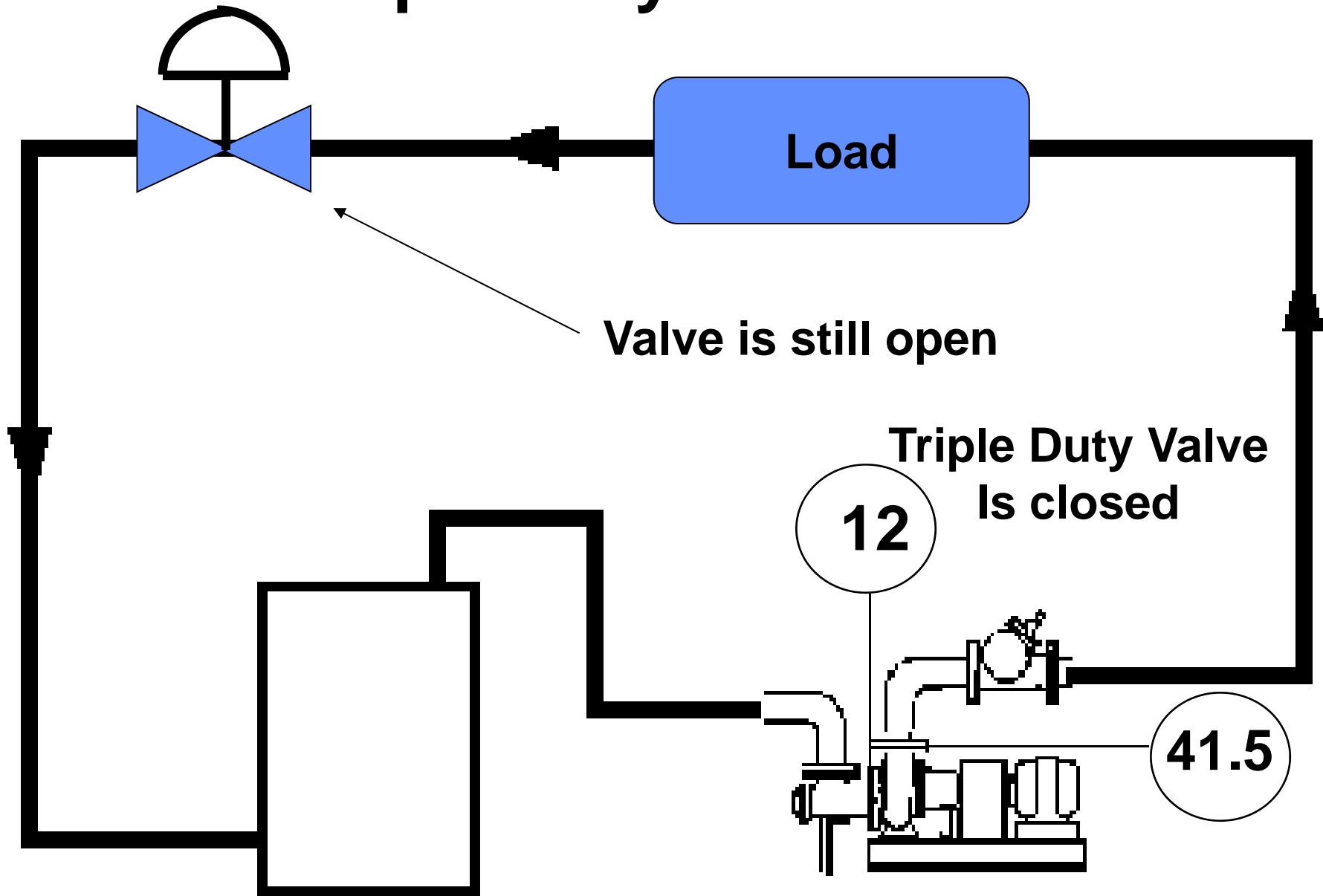
Impellers are trimmed in 1/8" increments to supply required capacity. Responsibility for final impeller sizing remains with ITT Bell & Gossett.

## Problem 2

You don't know the impeller size. But you know that if you close the Triple Duty Valve you can get the shutoff head, which will then lead you to the impeller size. The pressure rise across the pump with the 3D valve closed reads:

Suction Pressure	=	12.0 psi
Discharge pressure	=	<u>41.5 psi</u>

# Triple Duty Valve Closed



## Problem 2

Pressure differential across pump with the 3D valve closed:

Answer:

Differential Gauge Reading:

$$41.5\text{psi} - 12\text{psi} = 29.5\text{psi}$$

Convert to ft.:  $29.5\text{psi} \times 2.31\text{ft/psi} = 68\text{ft}$

Determine the:

Impeller Size

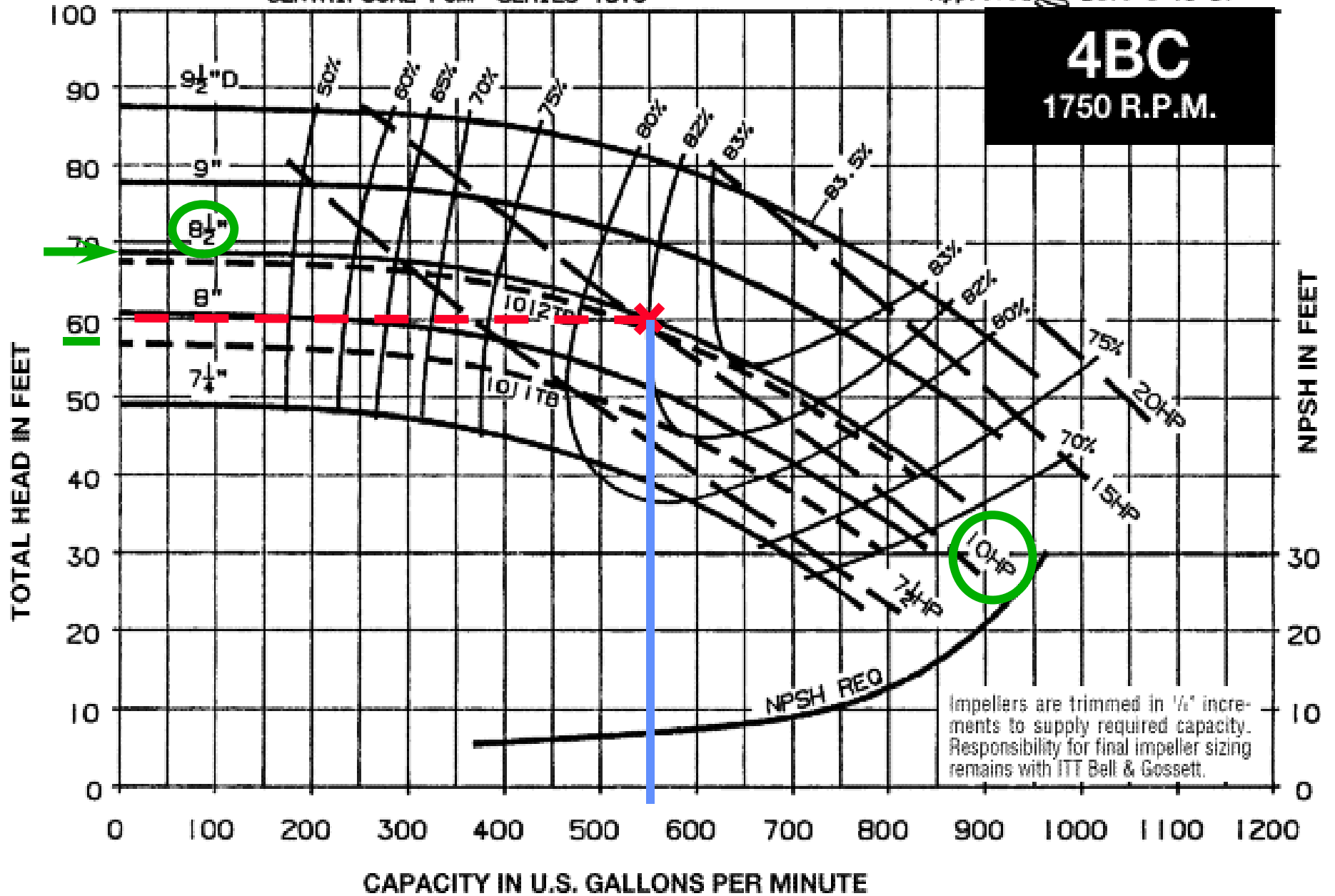
Flow Rate

Horsepower

CENTRIFUGAL PUMP SERIES 1510

Approved  Date 3-18-81

**4BC**  
1750 R.P.M.



## Problem 2

Determine the following:

Impeller Size	<u>8-1/2"</u>
Flow Rate	<u>550 GPM</u>
Horsepower	<u>10</u>
NOL	<u>15</u>

## Problem 3

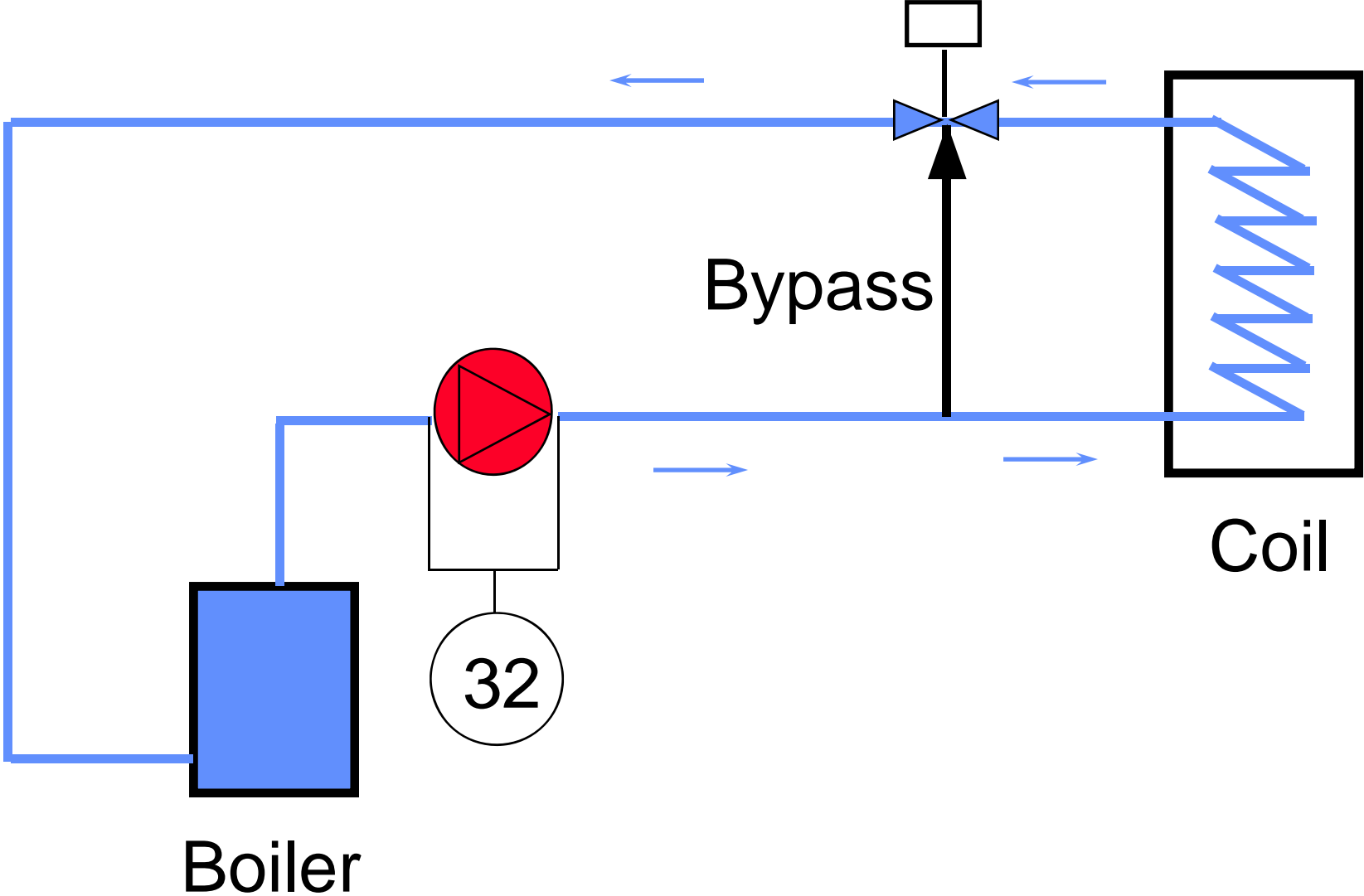
Your 2 HP, Series 1510 1-1/4BC regularly trips its circuit breaker. From the name plate you know you have an 8-1/2" impeller.

When the 3-way valve is fully open to the coil, the PD across the suction and discharge of the pump is 32 psi.

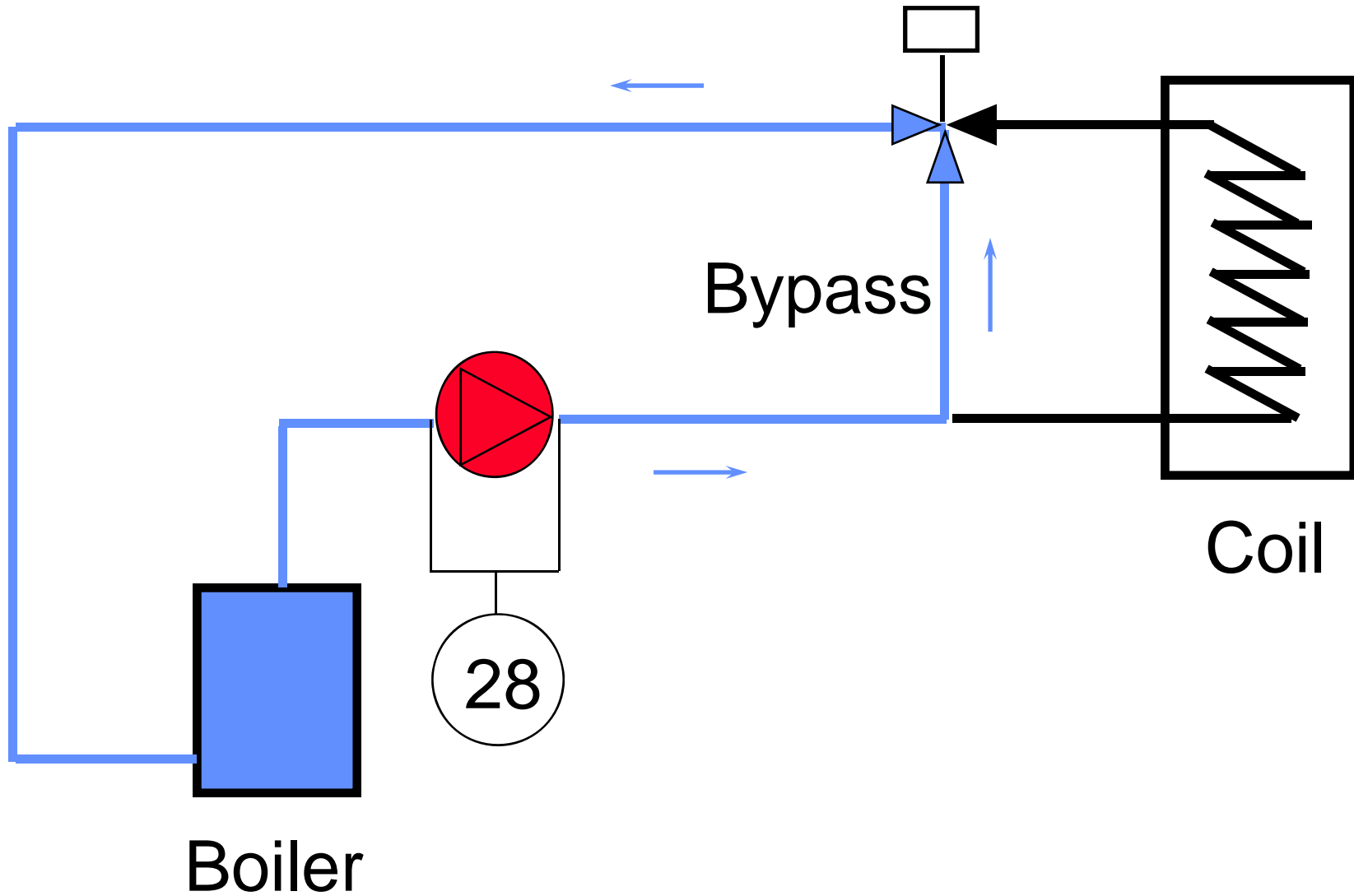
When the 3-way valve is open to bypass, the PD is 28 psi.

What's the flow through the coil? Bypass? What is the cause of the problem?

# Problem 3 - Coil



# Problem 3 - Bypass



## Problem 3

Answer:

**Coil**

Convert to ft.:

$$32\text{psi} \times 2.31\text{ft/psi} = 74\text{ft}$$

**Bypass**

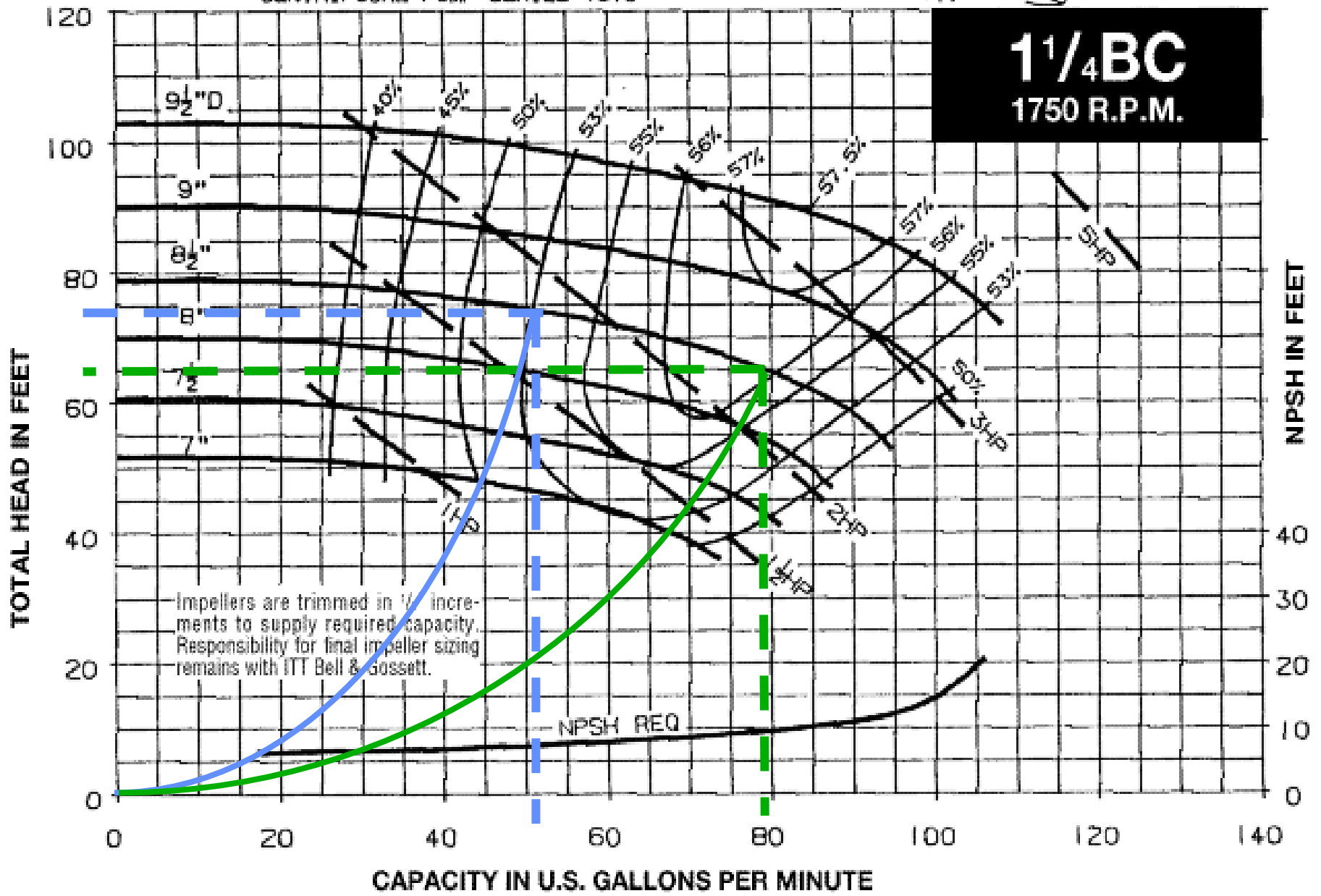
Convert to ft.:

$$28\text{psi} \times 2.31\text{ft/psi} = 65\text{ft}$$

CENTRIFUGAL PUMP SERIES 1510

Approved  Date 7-2-81

**1 1/4 BC**  
1750 R.P.M.



Coil      Bypass

## Problem 3

Answer:

Coil flow 74 Ft Hd (32 PSI) >> 51 GPM

Bypass flow 65 Ft Hd (28 PSI) >>79 GPM

What is the cause of the problem?

Solution?

## Problem 3

Cause of the problem:

Not enough PD across the bypass.

Pump rides out on its curve

Flow increases

Greater HP draw

Overload

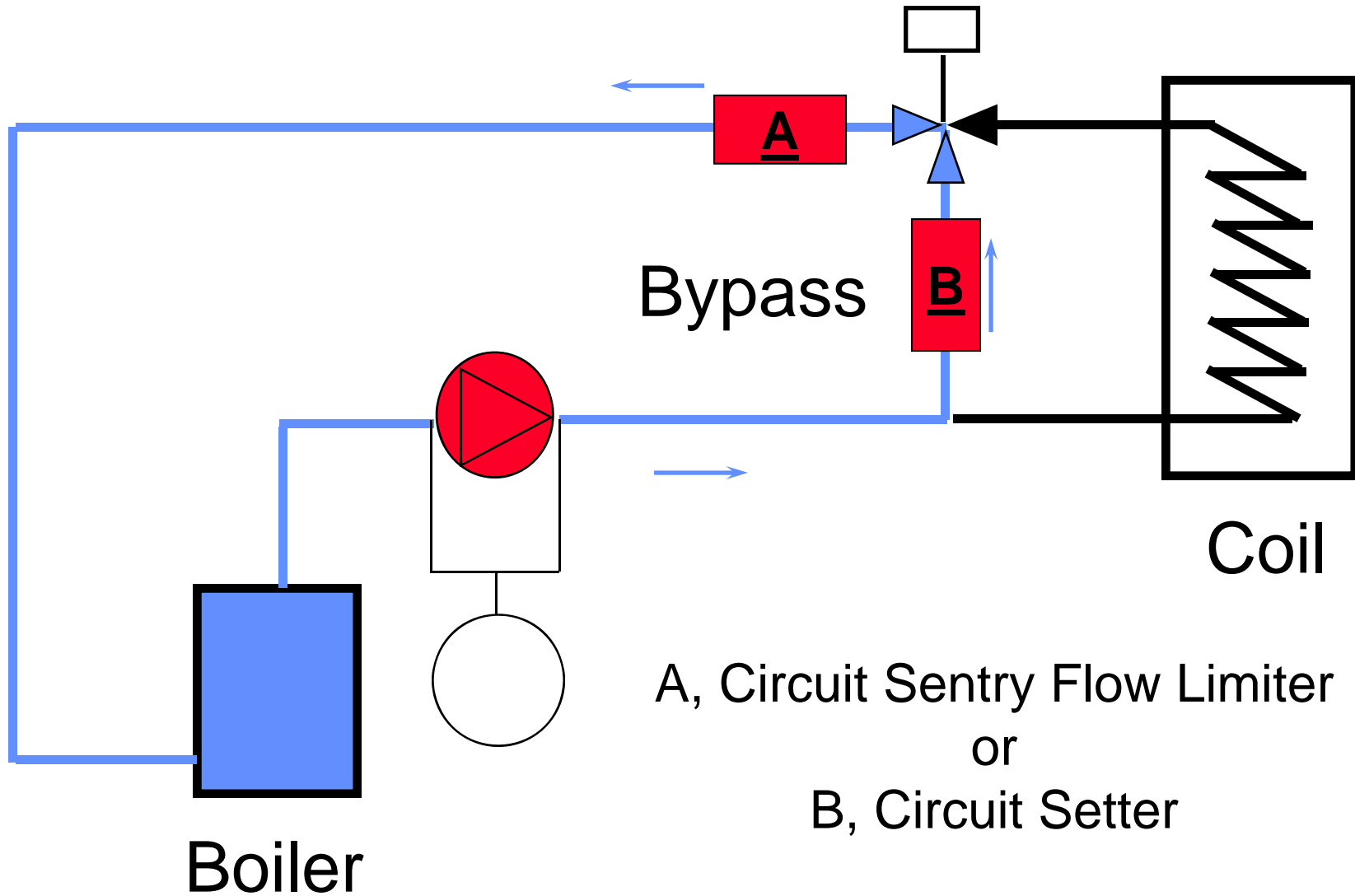
Solution?

Introduce PD across bypass equal to that of the coil.

Balance valve

Trim impeller - No

# Problem 3 - Solved



# Problem 4

The “new guy” calls you back from vacation early with a problem. There is sometimes a high pitched noise throughout the building and the motor sometimes cuts out.

You find:

- the pump running smoothly.
- voltage at the pump is normal, but the ammeter shows that the motor is drawing more than nameplate current.
- wiring isn't loose.
- pump rotates freely, no binding.

You consult with the design engineer. The pump was selected for 1300 gpm @ 179'. A 13-1/2" impeller was required. The motor selected was 75 Hp.

## Problem 4

Good thing you placed a gauge across the pump suction and discharge before you took vacation.

Checking to make sure that no one changed the impeller while you were on vacation last week, you close the 3D Valve for a few seconds.

Your PD = 86psi. (116 - 30)

Converting to ft:  $86\text{psi} \times 2.31\text{ft/psi} = 199'$

PERFORMANCE CHARACTERISTIC CURVE

FOR 5x6x15½ CENTRIFUGAL PUMP FIG. NO. V9CS

SPEED 1770 R.P.M.

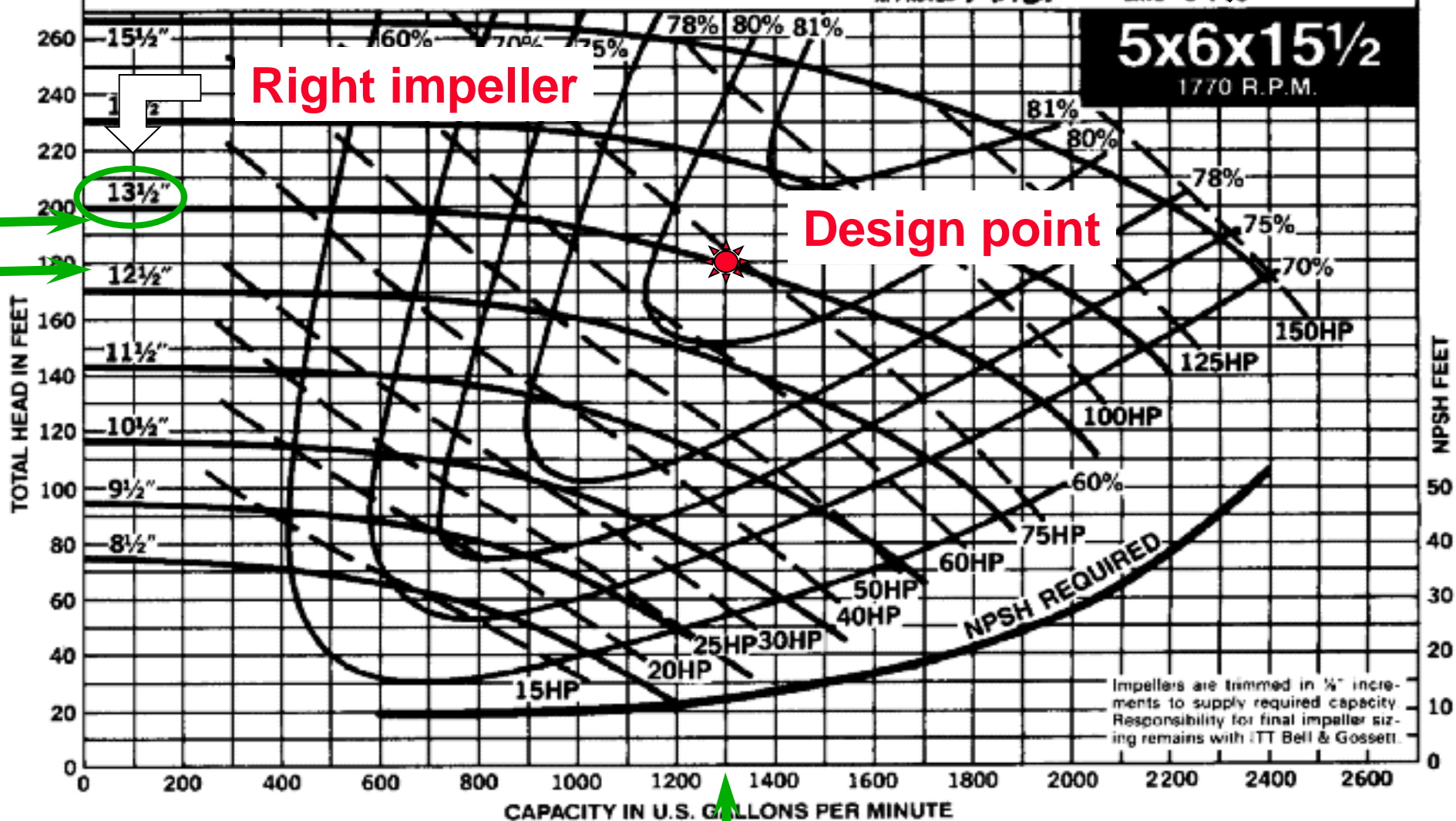
CURVES BASED ON SHOP TEST USING CLEAR COLD WATER AT A TEMPERATURE OF NOT OVER 85°F. PERFORMANCE IS GUARANTEED AT INDICATED OPERATING POINT ONLY.

Right pump

DATE 9-4-59

APPROVED R.B.

5x6x15½  
1770 R.P.M.



# Problem 4

The impeller checks out.

Knowing you shouldn't dead head a pump for too long, you return the 3D Valve back to its original position.

Now you take another reading. In normal operation, the PD = 67 psi. (97 psi – 30 psi)

Converting to ft:  $67 \text{ psi} \times 2.31 \text{ ft/psi} = 155'$

Strange, the engineer specified 1300 gpm @ 179'.

PERFORMANCE CHARACTERISTIC CURVE

FOR 5x6x15½ CENTRIFUGAL PUMP FIG. NO. VSCS

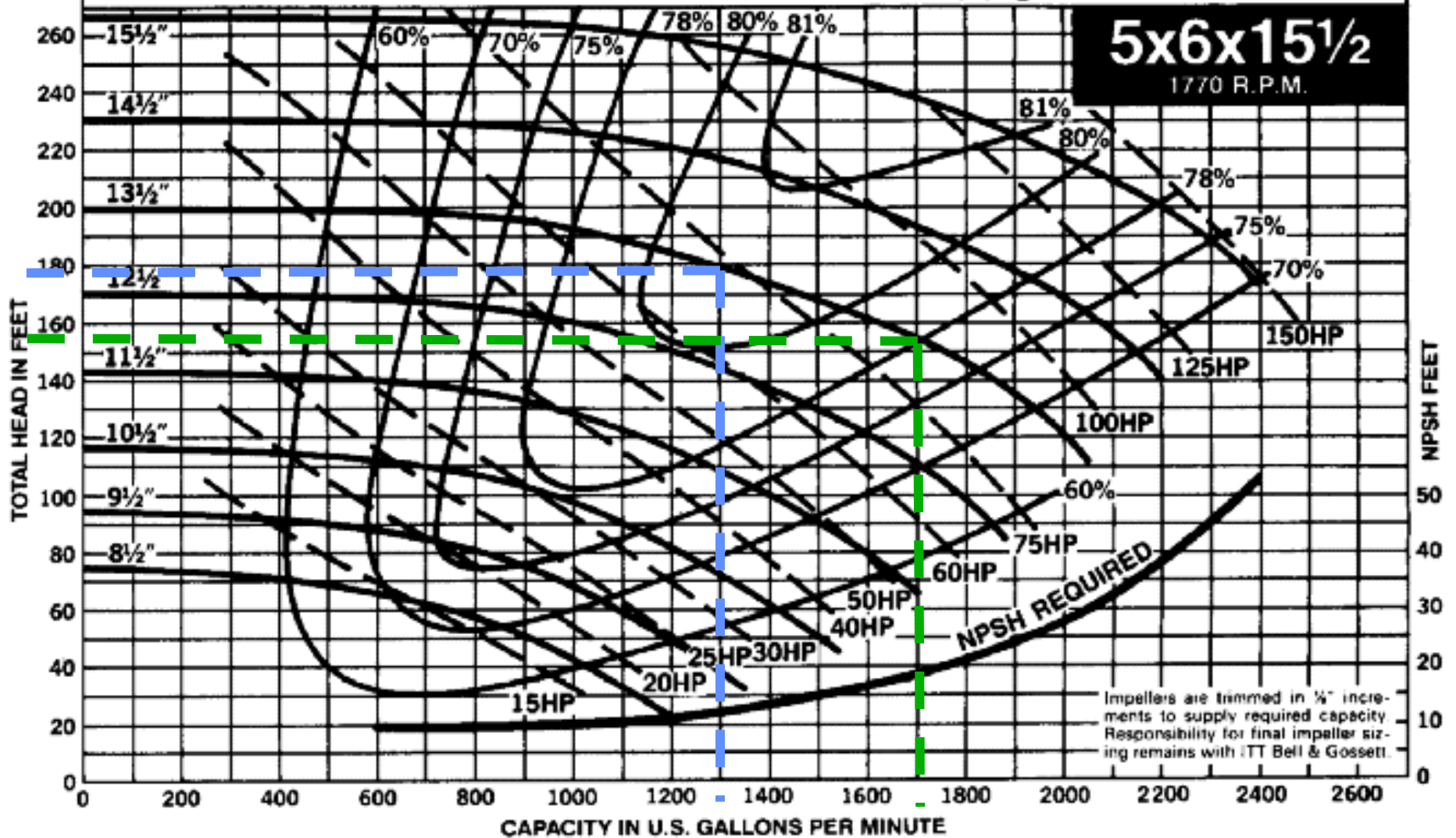
SPEED 1770 R.P.M.

CURVES BASED ON SHOP TEST USING CLEAR COLD WATER AT A TEMPERATURE OF NOT OVER 85°F. PERFORMANCE IS GUARANTEED AT INDICATED OPERATING POINT ONLY.

APPROVED *R.T.B.*

DATE 9-4-79

**5x6x15½**  
1770 R.P.M.



Design Actual

Impellers are trimmed in ¼" increments to supply required capacity. Responsibility for final impeller sizing remains with ITT Bell & Gossett.

## **Problem 4**

Why does the motor cut out at times?

What is the cause of the noise?

What do you recommend for a solution?

What should you do to the new guy?

# Problem 4

Motor cut out:

Actual PD lower than designed

Greater GPM

Greater HP draw

Overloaded motor.

Noise:

Fluid Velocity in Pipe

Pump Noise:

Greater GPM

Greater NPSHR

It could be that  $NPSHR > NPSHA$

Cavitation

PERFORMANCE CHARACTERISTIC CURVE

FOR 5x6x15½ CENTRIFUGAL PUMP FIG. NO. VSCS

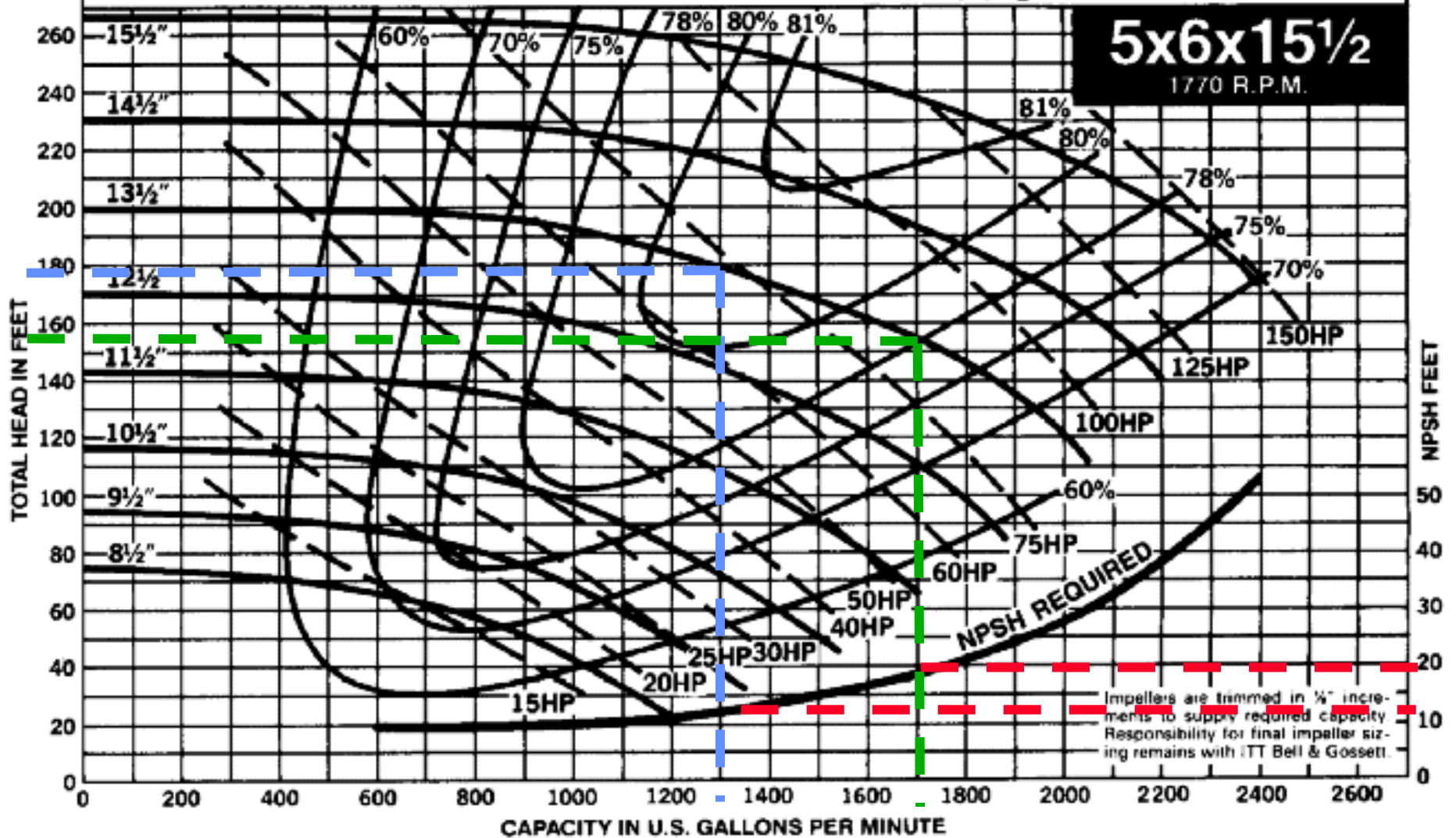
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APPROVED *R.T.B.*

DATE 9-4-79

**5x6x15½**  
1770 R.P.M.



Design Actual

## Problem 4

Recommendation:

- Close down on the 3D Valve
  - May substitute one problem for another
  - May damage the valve
- Trim impeller, then throttle 3D Valve
- Any other ideas?

New Guy:

Training

Send him to The Little Red Schoolhouse<sup>®</sup>

If that doesn't work, then ...

PERFORMANCE CHARACTERISTIC CURVE

FOR 5x6x15½ CENTRIFUGAL PUMP FIG. NO. VSCS

SPEED 1770 R.P.M.

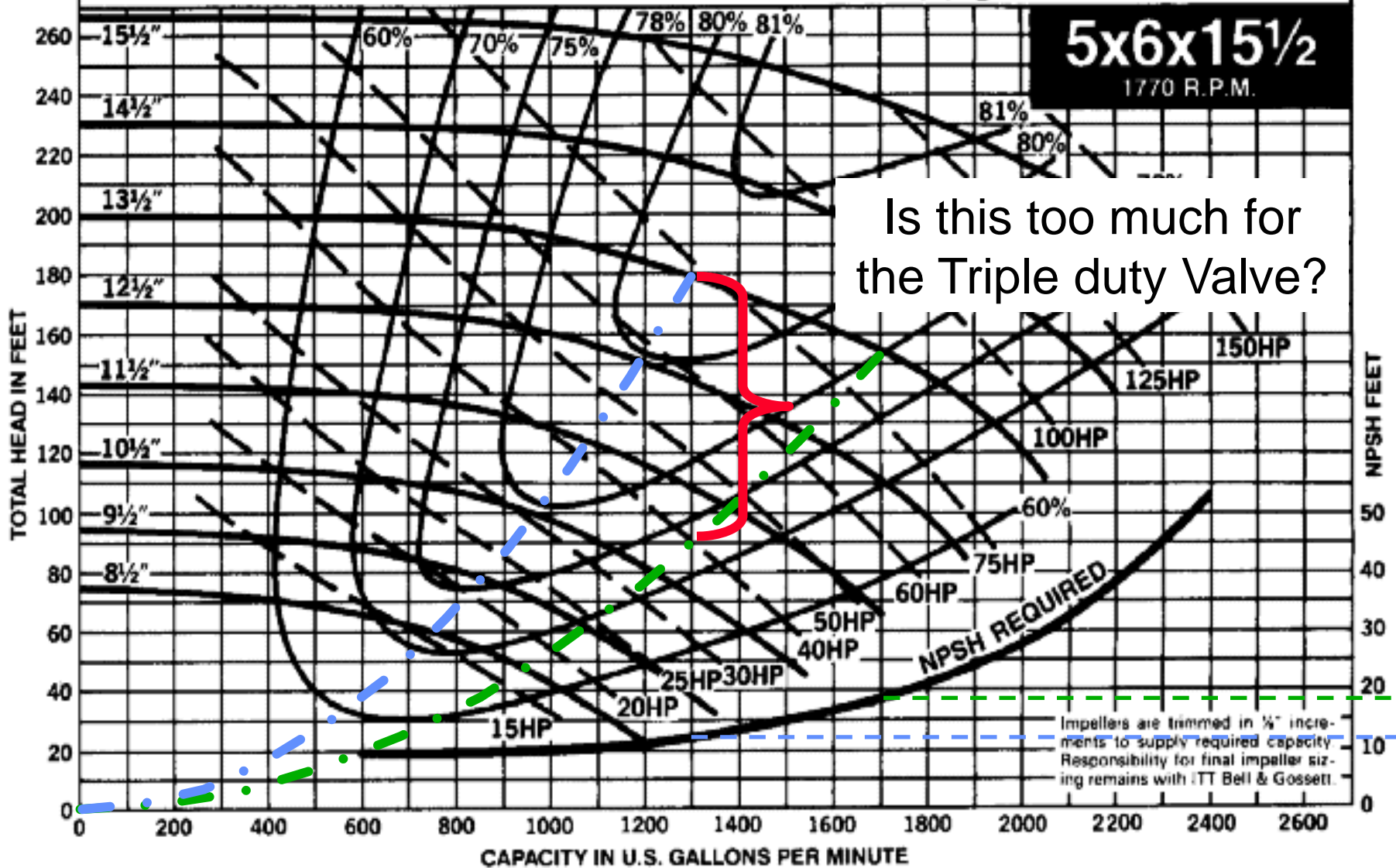
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APPROVED *R.T.B.*

DATE 9-4-79

**5x6x15½**

1770 R.P.M.



# Avoid Pump Cavitation

- NPSH Required by the pump
  - Head loss in the impeller.
  - Impeller design, materials.
  - Flow rate.

- NPSH Available from a closed system
  - Static head
  - System pressurization



**Questions?**

# Additional Resources



- <http://bellgossett.com/training-education>
  - On-Line Training
  - Seminar Information
- AWS Newsletter
- Our Representative in your area.



**Bell & Gossett**

a **xylem** brand